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## **APPLICATION**

## **FOR**

## UNITED STATES LETTERS PATENT

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APPLICANT:

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PRESTON PARKER

#### **APPENDIX 2**

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### The Jet Pump

One practical use of the fluid jet is to pump fluids to a higher pressure by use of a jet of fluid injected into a pipe of moving fluid. Such a *jet pump* is illustrated in figure 5.6 which shows a jet of velocity  $V_a$  and area  $A_a$  aligned with the axis of a pipe of area A at a point where the pipe flow velocity is  $V_1$  and the pressure is  $P_1$ . At a distance downstream, where the two streams have completely mixed, the velocity is  $V_2$ , and the pressure  $P_2$  is greater than  $P_1$ . The amount of the pressure rise  $P_2 - P_1$  depends upon the velocities  $V_1$  and  $V_2$  and the area ratio  $A_4/A$  in a manner that may be found by applying mass and momentum conservation to the fluid in the control volume shown in figure 5.6.

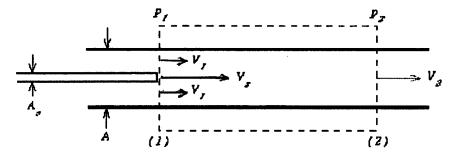


Figure 5.6: A jet pump consists of a coaxial jet of high speed fluid injected into a pipe of lower speed fluid. The mixing of the two streams produces a rise in pressure downstream.

We will consider the case for which the jet fluid and the pumped fluid are both incompressible and have the same density P. Applying mass conservation to the steady flow of fluid across the control surface of figure  $\underline{5.6}$ ,

$$\rho A V_2 = \rho (A - A_a) V_1 + \rho A_a V_a$$

Next use the linear momentum equation 5.11 for the same control volume, but assume that the viscous force on the pipe walls is negligible ( $\tau = 0$ ):

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$$\frac{d}{dt} \iiint_{\mathcal{V}} \rho \mathbf{V} \, d\mathcal{V} + (\dot{m} \mathbf{V})_{out} - (\dot{m} \mathbf{V})_{in}$$

$$= \iint_{\mathcal{S}} (-p\mathbf{n}) \, d\mathcal{S} + \iint_{\mathcal{S}} d\mathcal{S} + \iiint_{\mathcal{V}} \rho \mathbf{g} \, d\mathcal{V} + \Sigma \mathbf{F}_{ex}$$

$$0 + \rho A V_{2}^{2} - \rho (A - A_{e}) V_{1}^{2} - \rho A_{e} V_{e}^{2}$$

$$= (p_{1} - p_{2}) A + 0 + 0 + 0$$

Eliminating  $V_2$  between these two equations and solving for the pressure rise,

$$p_2 - p_1 = \frac{A_a}{A} \left( 1 - \frac{A_a}{A} \right) \rho (V_a - V_1)^2 \tag{5.24}$$

The maximum pressure rise that we could expect would be that for inviscid flow of the jet decelerating from the speed  $V_a$  to  $V_2 = V_a A_a / A$ , or a pressure rise of  $(pV_a^2/2)(1 - A_a^2/A^2)$ . Dividing equation 5.24 by this pressure rise, we have a dimensionless form of the jet pump equation:

$$\frac{p_1 - p_2}{\frac{1}{2}\rho V_a^2 \left[1 - (A_a/A)^2\right]} = 2\left(\frac{A_a/A}{1 + A_a/A}\right) \left(1 - \frac{V_1}{V_a}\right)^2$$
 (5.25)

Since  $A_a/A \le 1$  and  $V_1/V_a \le 1$ , the right side of equation 5.25 is always less than one.

The jet pump allows us to pump a greater volume flow rate  $(V_1[A - A_n])$  than that needed to supply the jet  $(V_nA_n)$ , albeit with a lower pressure rise than that needed for the jet supply.

#### Example 5.12

A jet pump consists of a jet of diameter  $D_s = 1$  in inside a pipe of diameter D = 3 in. The jet volumetric flow rate  $Q_s$  is 100 GPM (gallons per minute). Calculate the pressure rise in the jet pump when the volumetric flow rate  $Q_1$  is 500 GPM.

#### Solution

In SI units, the flow areas and flow rates are:

 $Q_1 = 5 Q_s = 3.154 E(-2) m^3/s$ 

$$A_s = \frac{\pi}{4} (2.54E(-2)m)^2 = 5.067E(-4)m^2; \qquad A = 9A_s = 4.560E(-3)m^2$$

$$Q_s = \frac{100 \text{ gal}}{\text{min}} \times \frac{3.785E(-3)m^3}{\text{gal}} \times \frac{\text{min}}{60 \text{ s}} = 6.308E(-3)m^3/s;$$

and the velocities  $V_1$  and  $V_5$  are:

$$V_1 = \frac{Q_1}{A - A_s} = \frac{3.154E(-2)m^3/s}{4.560E(-3)m^2 - 5.067E(-4)m^2} = 7.781 m/s$$

$$V_s = \frac{Q_s}{A_s} = \frac{6.308E(-3)m^3/s}{5.067E(-4)m^2} = 12.45 m/s$$

Substituting these values in equation 5.24,

$$p_2 - p_1 = \frac{1}{9} \left( 1 - \frac{1}{9} \right) (1E(3)kg/m^3)(12.45 \, m/s - 7.781 \, m/s)^2 = 2.153E(3) \, Pa$$

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Marie Hwang Fri Mar 1 16:42:21 EST 1996